

JC07 Rec'd PCT/PTO 26 OCT 2001  
10/009627

Express Mail Label No. EK 943404951 US  
Date Mailed: October 26, 2001

100745-7 / Miura 214-KGB  
Client's Ref.: F-E-3

#2/  
/a

IN THE UNITED STATES PATENT AND TRADEMARK OFFICE

APPLICANTS : ISAMU UEMASU ET AL  
SERIAL NO. : TO BE ASSIGNED  
FILED : HERewith  
FOR : METHOD AND EQUIPMENT FOR CONTINUOUS AND  
SELECTIVE INCLUSION SEPARATION  
ART UNIT : TO BE ASSIGNED  
EXAMINER : TO BE ASSIGNED

October 26, 2001

Hon. Commissioner of Patents  
Washington, D.C. 20231

**PRELIMINARY AMENDMENT**

SIR:

Prior to examination, please amend the above-identified application as follows:

IN THE DESCRIPTION:

Last paragraph beginning on page 7, please change as follows:

Organic solvents hardly soluble in water and hardly capable of forming an inclusion complex with a cyclodextrin are preferred as the organic solvent for use in dissociating and extracting a compound entrapped in the aqueous cyclodextrin phase from the cyclodextrin.

10009627-152601

Examples of such organic solvents include ethers such as diethyl ether, diisopropyl ether, and diisoamyl ether; hydrocarbons such as liquefied propane gas, L P G, liquefied butane gas, pentanes, hexanes, heptanes, and mesitylene; and halogenated hydrocarbons such as dichloromethane. Incidentally, in the case of an extraction solvent highly volatile with a boiling point of at least ordinary temperature and comparatively easily soluble in the aqueous solution of cyclodextrin like diethyl ether, it is preferred to repeat at suitable time intervals the procedure of effecting extraction by stirring for a period of a few seconds to several tens of seconds after addition of the extraction solvent and then recovering the resulting organic solvent layer. In this case, as the extraction solvent in continuing the operation after recovery of the solvent layer, either virgin solvent may be replenished, or the solvent separated from the compound(s) as the object(s) of separation through distillation or the like of the solvent layer may be reused.

Last paragraph beginning on page 8, please change as follows:

When a low-boiling solvent boiling below ordinary temperature, e.g., liquefied petroleum gas (LPG), liquefied propane gas or liquefied butane gas, is used as the extraction solvent, a raw material containing a compound(s) to be separated therefrom and an aqueous solution of inclusion-complexing agent are placed in a reaction vessel such as a U-shaped tube or an H-shaped tube in an inclusion separator provided with a pressurizing means, e.g., an apparatus having a reaction vessel placed in an autoclave, and the low-boiling solvent is then placed in the reaction vessel under pressure, followed by stirring to perform a separation operation. After the separation operation, the separator is depressurized to recover the vapor of the low-boiling

solvent. During the course of depressurization, heat being generated during liquefaction of the low-boiling solvent vapor through pressurization may be utilized as an (ancillary) means for preventing temperature drop of the organic phase and the aqueous phase in the reaction vessel in keeping with evaporation of the low-boiling solvent (means particularly for preventing the aqueous phase from freezing). The liquefied low-boiling solvent can be reused as the extraction solvent. The extracted organic compound(s) remaining in the reaction vessel is recovered.

Alternatively, the organic phase after the extraction operation may be first withdrawn from the reaction vessel into a pressure vessel from which the low-boiling solvent vapor is recovered, instead of direct recovery of the low-boiling solvent vapor from the reaction vessel. In this case as well, heat being generated during pressurization and liquefaction of the low-boiling solvent vapor may of course be used as an (ancillary) means for preventing temperature drop of the residual organic phase(s) and the aqueous phase. Advantages of using a low-boiling solvent boiling below ordinary temperature lie in that a great difference in boiling point between a compound as an object of separation like axylene isomer and an extraction solvent hardly allows the low-boiling solvent to mix in the separated compound, and in that a large-scale and elaborate distillation apparatus may be dispensed with in performing an industrial separation process according to the present invention.

Page 17, Example 5, please change as follows:

#### Example 5

250 ml of a 10 wt.% aqueous solution of a glucosyl-  $\alpha$  - cyclodextrin mixture was placed

in a U-shaped tube. 6 ml of mixed xylene (commercially available product) was placed in one vertical tube of the U-shaped tube while 6 ml of n-hexane was placed in the other vertical tube. Stirring was effected in such a manner that the xylene phase did not mix with the hexane phase. The composition of xylene isomers extracted in the n-hexane phase after 2 hours is shown in Table 5.

Page 19, Example 10, please change as follows:

#### Example 10

250 ml of a 10 wt. % aqueous solution of a glucosyl-  $\alpha$  -cyclodextrin mixture was placed in an H-shaped tube. 10 ml of mixed xylene (commercially available product) was placed in one vertical tube of the H-shaped tube while 5 ml of dichloromethane was placed in the other vertical tube. Vigorous stirring was effected, provided that the horizontal pipe portion of the H-shaped tube was partitioned with filter paper. The composition of xylene isomers extracted in the dichloromethane phase after 1 hour is shown in Table 10.

#### IN THE CLAIMS:

Please amend claims 3 and 5 as follows:

3. A continuous and selective inclusion separation method as claimed in claim 1, characterized in that said inclusion-complexing agent is a cyclodextrin(s).
5. A continuous and selective inclusion separation method as claimed in claim 1, characterized in that at least part of a solution as the organic phase containing a

compound extracted thereinto as an object of separation is withdrawn and distilled to concentrate said compound, and the organic solvent separated by distillation is returned back to the reaction system and reused as the extraction solvent.

REMARKS

It is not believed that the amendments above affects the scope of the claims. The claims have been amended to eliminate multiple dependencies, and place them in better form for U.S. examination.

Support for the specification changes is as follows:

In connection with the changes on page 8, various dictionaries teach that the abbreviation "LPG" refers to liquefied petroleum gas. It is not believed that this amendment effects the scope of claims.

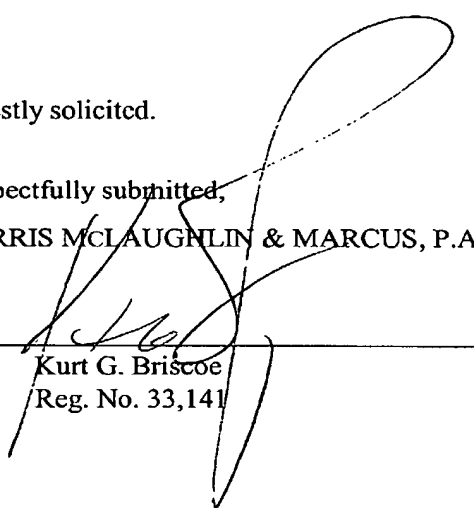
In connection with the change on page 17, see "n-hexane" on page 17, lines 5 and 8.

In connection with the change on page 19, see page 11 lines 27-29 together with Fig. 5 and page 4 line 15 (and page 5 line 9).

Early and favorable action is earnestly solicited.

Respectfully submitted,  
NORRIS MCLAUGHLIN & MARCUS, P.A.

By

  
Kurt G. Briscoe  
Reg. No. 33,141

KGB:ja  
220 East 42<sup>nd</sup> Street  
30<sup>th</sup> Floor  
New York, New York 10017  
Tel.: (212) 808-0700

## MARK-UP SHOWING THE CHANGES MADE IN THE DESCRIPTION

Last paragraph beginning on page 7, please change as follows:

Organic solvents hardly soluble in water and hardly capable of forming an inclusion complex with a cyclodextrin are preferred as the organic solvent for use in dissociating and extracting a compound entrapped in the aqueous cyclodextrin phase from the cyclodextrin. Examples of such organic solvents include ethers such as diethyl ether, diisopropyl ether, and diisoamyl ether; hydrocarbons such as [liquefied propane gas (LPG)] **liquefied propane gas, L P G**, liquefied butane gas, pentanes, hexanes, heptanes, and mesitylene; and halogenated hydrocarbons such as dichloromethane. Incidentally, in the case of an extraction solvent highly volatile with a boiling point of at least ordinary temperature and comparatively easily soluble in the aqueous solution of cyclodextrin like diethyl ether, it is preferred to repeat at suitable time intervals the procedure of effecting extraction by stirring for a period of a few seconds to several tens of seconds after addition of the extraction solvent and then recovering the resulting organic solvent layer. In this case, as the extraction solvent in continuing the operation after recovery of the solvent layer, either virgin solvent may be replenished, or the solvent separated from the compound(s) as the object(s) of separation through distillation or the like of the solvent layer may be reused.

Last paragraph beginning on page 8, please change as follows:

When a low-boiling solvent boiling below ordinary temperature, e.g., [liquefied petroleum gas such as liquefied propane gas (LPG)] **liquefied petroleum gas (LPG), liquefied propane gas** or liquefied butane gas, is used as the extraction solvent, a raw material containing a compound(s) to be separated therefrom and an aqueous solution of inclusion-complexing agent are placed in a reaction vessel such as a U-shaped tube or an H-shaped tube in an inclusion separator provided with a pressurizing means, e.g., an apparatus having a reaction vessel placed

10009627-102654

in an autoclave, and the low-boiling solvent is then placed in the reaction vessel under pressure, followed by stirring to perform a separation operation. After the separation operation, the separator is depressurized to recover the vapor of the low-boiling solvent. During the course of depressurization, heat being generated during liquefaction of the low-boiling solvent vapor through pressurization may be utilized as an (ancillary) means for preventing temperature drop of the organic phase and the aqueous phase in the reaction vessel in keeping with evaporation of the low-boiling solvent (means particularly for preventing the aqueous phase from freezing). The liquefied low-boiling solvent can be reused as the extraction solvent. The extracted organic compound(s) remaining in the reaction vessel is recovered. Alternatively, the organic phase after the extraction operation may be first withdrawn from the reaction vessel into a pressure vessel from which the low-boiling solvent vapor is recovered, instead of direct recovery of the low-boiling solvent vapor from the reaction vessel. In this case as well, heat being generated during pressurization and liquefaction of the low-boiling solvent vapor may of course be used as an (ancillary) means for preventing temperature drop of the residual organic phase(s) and the aqueous phase. Advantages of using a low-boiling solvent boiling below ordinary temperature lie in that a great difference in boiling point between a compound as an object of separation like axylene isomer and an extraction solvent hardly allows the low-boiling solvent to mix in the separated compound, and in that a large-scale and elaborate distillation apparatus may be dispensed with in performing an industrial separation process according to the present invention.

Page 17, Example 5, please change as follows:

#### Example 5

250 ml of a 10 wt.% aqueous solution of a glucosyl-  $\alpha$  - cyclodextrin mixture was placed in a U-shaped tube. 6 ml of mixed xylene (commercially available product) was placed in one vertical tube of the U-shaped tube while 6 ml of n-hexane was placed in the other vertical tube. Stirring was effected in such a manner that the xylene phase did not mix with the [heptane] hexane phase. The composition of xylene isomers extracted in the n-hexane phase after 2 hours is shown in Table 5.

Page 19, Example 10, please change as follows:

Example 10

250 ml of a 10 wt. % aqueous solution of a glucosyl-  $\alpha$  -cyclodextrin mixture was placed in an H-shaped tube. 10 ml of mixed xylene (commercially available product) was placed in one vertical tube of the H-shaped tube while 5 ml of dichloromethane was placed in the other vertical tube. Vigorous stirring was effected, provided that the [bottom] horizontal pipe portion of the H-shaped tube was partitioned with filter paper. The composition of xylene isomers extracted in the dichloromethane phase after 1 hour is shown in Table 10.

10009827-100004



**MARK-UP SHOWING THE CHANGES MADE IN THE PREVIOUS CLAIM TO YIELD  
THE CLAIM AS AMENDED ABOVE**

3. A continuous and selective inclusion separation method as claimed in [claim 1 or 2] **claim 1**, characterized in that said inclusion-complexing agent is a cyclodextrin(s).
5. A continuous and selective inclusion separation method as claimed in [ any one of claims 1 to 4] **claim 1**, characterized in that at least part of a solution as the organic phase containing a compound extracted thereinto as an object of separation is withdrawn and distilled to concentrate said compound, and the organic solvent separated by distillation is returned back to the reaction system and reused as the extraction solvent.